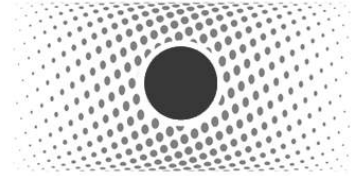




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Institute for Chemical Engineering,  
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# Particularities of the combustion chamber in a dual fluidized bed biomass gasifier

*IEA-FBC Workshop  
Combustion and gasification in FBC*

*May 20, 2006, Vienna*

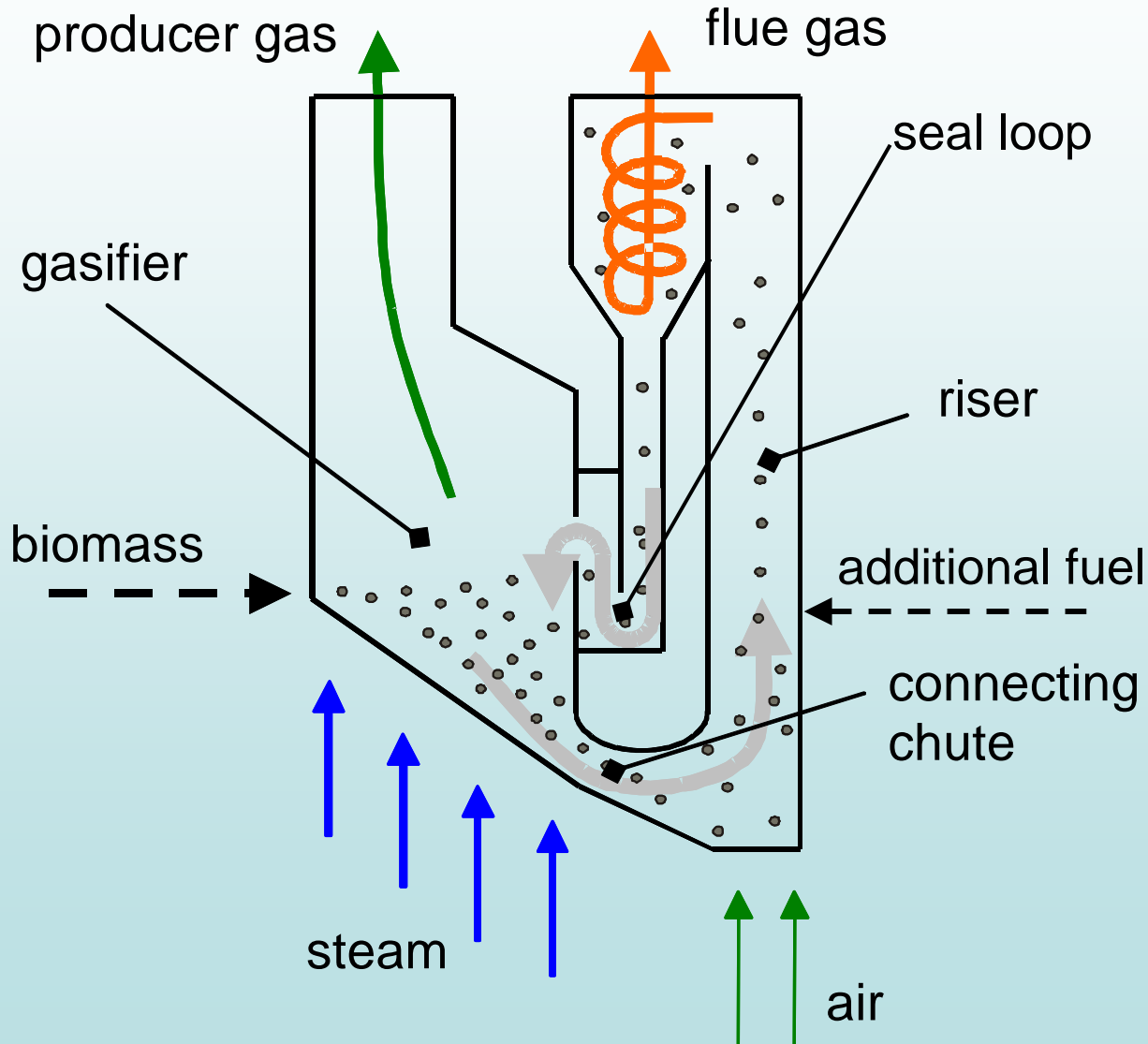
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Vienna University of Technology  
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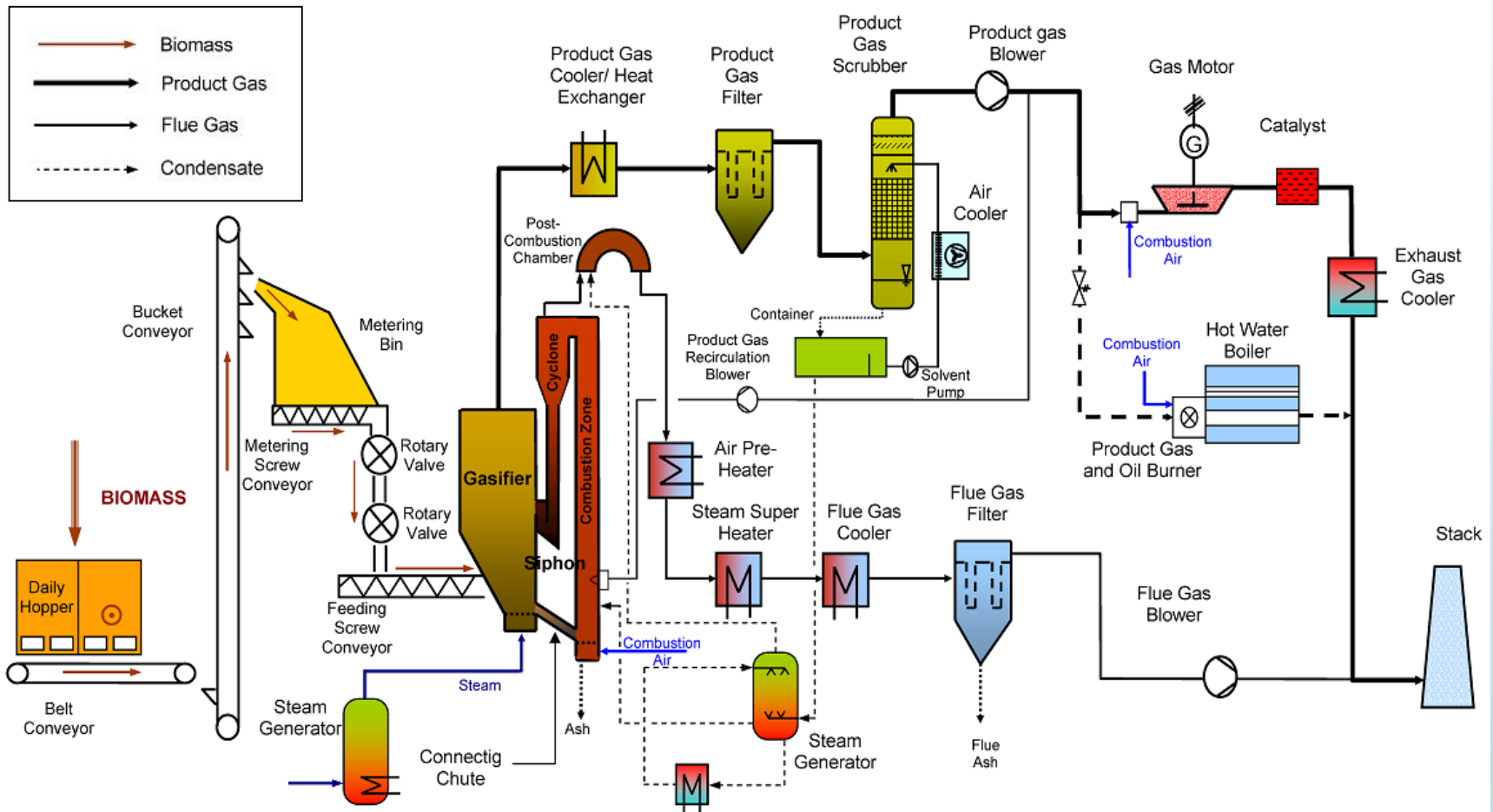
# Outline

- The dual fluidized bed gasification process
- The 8 MW CHP plant in Güssing
- Combustion chamber and flue gas line
- Air preheater design
- Conclusions

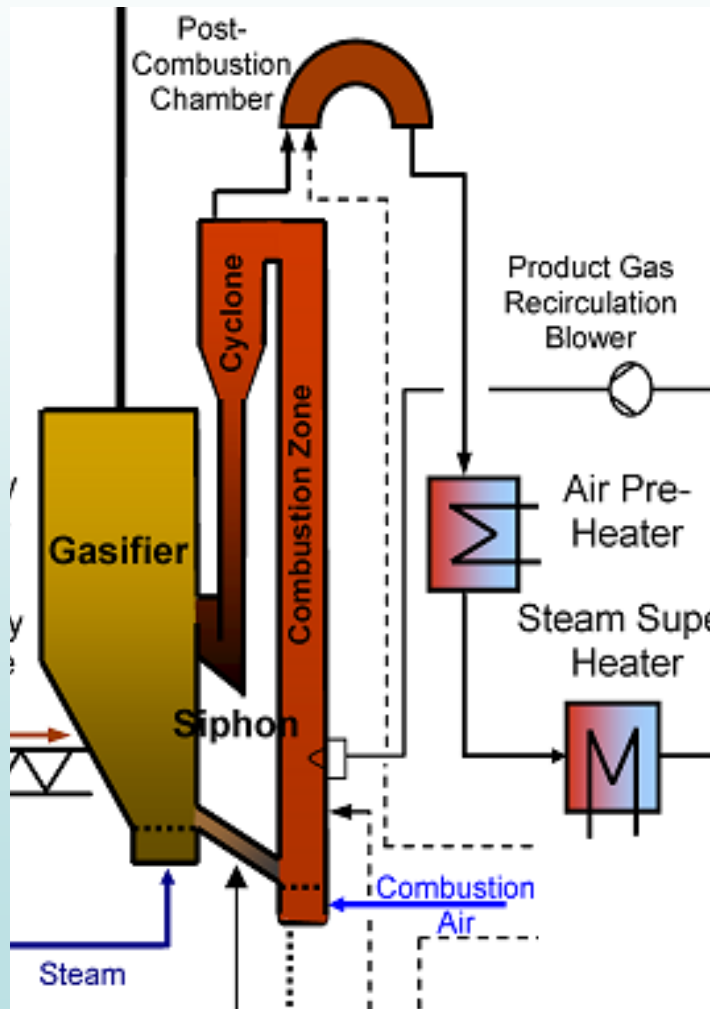
# Dual fluidized bed gasification



# The dual fluidized bed steam gasification CHP plant in Güssing/Austria



# Combustion chamber and flue gas line



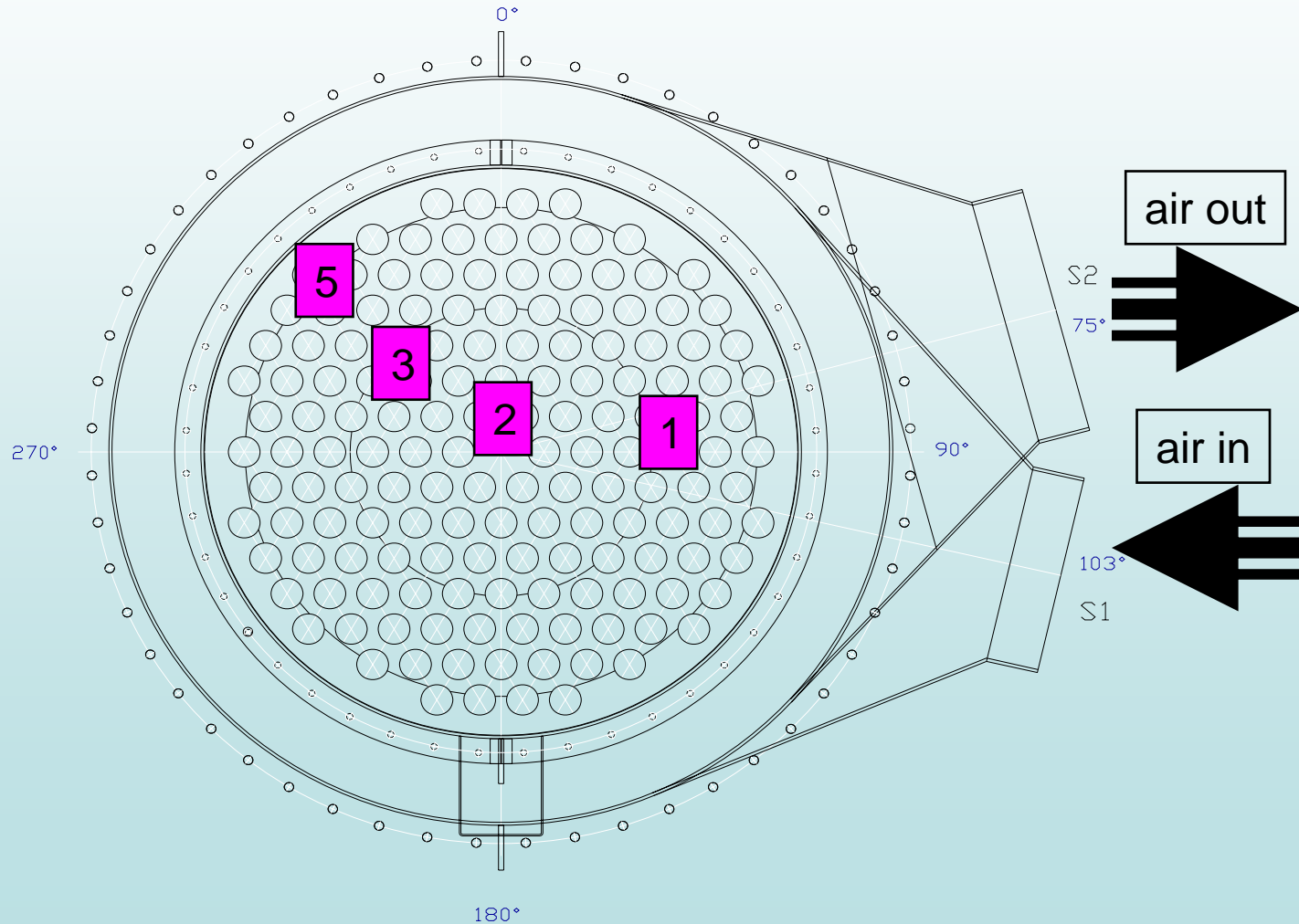
- riser height 9 m, 0.5 m<sup>2</sup> riser section
- co-combustion of
  - biomass char
  - spent tar solvent/water
  - producer gas (recycled)
- riser fuel power 2...4 MW
- **recent observations:**
  - significant part of the combustion shifted to post combustion chamber
  - depositions on the air preheater surfaces

# Operating conditions of the air preheater

Co-Current Flue gas in tubes design:

air inlet temperature:	ca. 60°C
air outlet temperature:	ca. 400°C
flue gas inlet temperature:	800-900°C
air flow rate:	4000-5000 Nm <sup>3</sup> /h
flue gas flow rate:	ca. 7000Nm <sup>3</sup> /h
dust content:	30-50g/Nm <sup>3</sup>

# Heat exchanger design









# Melting behaviour of deposits



600°C



700°C



800°C



900°C



1000°C



1100°C



1200°C



1300°C



1330°C



1350°C

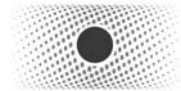


1380°C



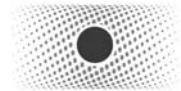
1400°C

# Elementar comp. deposits



	Pr1-04	Pr1-05	Pr1-06
Element	At%	At%	At%
C	5,24	7,34	15,61
O	41,43	32,67	33,71
Na	2,61	n.d.	n.d.
Mg	4,16	22,84	14,12
Al	9,25	1,44	1,25
Si	25,88	7,22	4,19
P	n.d.	0,64	0,83
K	4,48	5,02	11,69
Ca	6,48	20,15	17,42
Mn	0,13	0,58	0,37
Fe	0,35	2,1	0,78
<b>Total</b>	<b>100</b>	<b>100</b>	<b>100</b>

# Cristallographic Anal.



	mol%	Limestone	Ash	Smpl. 1	Smpl. 5
Quartz	SiO <sub>2</sub>	0,5	0,4	4,8	
Calcite	CaCO <sub>3</sub>	21,5	23,6		9,9
Dolomite	CaMg(CO <sub>3</sub> ) <sub>2</sub>	78,0			
CaO	CaO		18,4		2,5
Periclase	MgO		18,5	57,8	23,9
Portlandite	Ca(OH) <sub>2</sub>		3,8		
Forsterite	Mg <sub>2</sub> SiO <sub>4</sub>		19,8		
Ca-Silikat	Ca <sub>6</sub> Si <sub>3</sub> O <sub>12</sub>		15,5		
Antigorite-M	Mg <sub>26</sub> Si <sub>14</sub> O <sub>80</sub>			2,4	
Tilleyite	Ca <sub>5</sub> Si <sub>2</sub> C <sub>2</sub> O <sub>13</sub>			17,9	
Fairchildite	K <sub>2</sub> CaC <sub>2</sub> O <sub>18</sub>			17,1	4,2
Monticellite	MgCaSiO <sub>4</sub>				8,9
Monticellite	MgCaSiO <sub>4</sub>				3,7
Spurrite	Ca <sub>5</sub> Si <sub>2</sub> C <sub>10</sub> O <sub>11</sub>				47,0

# Interpretation

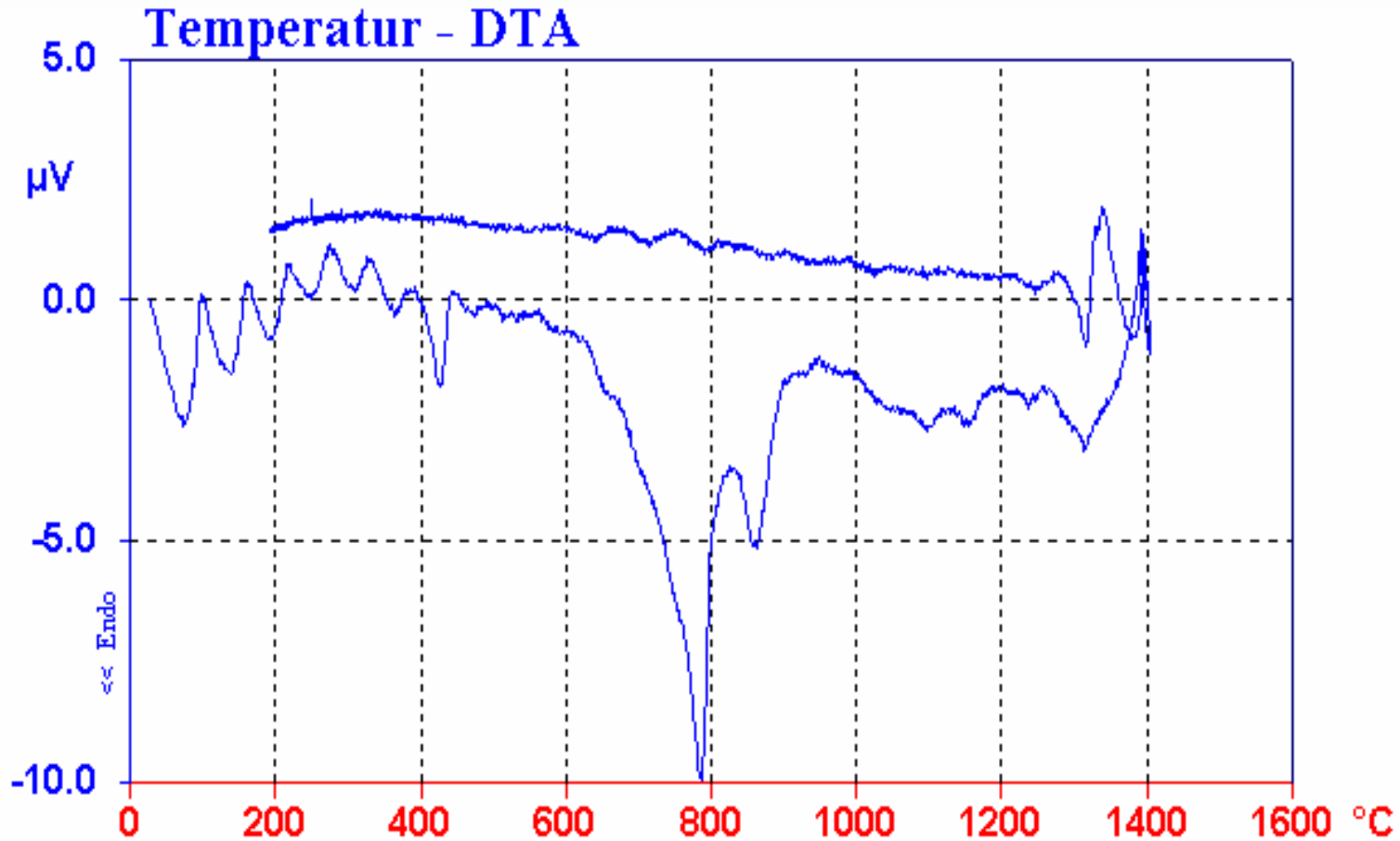
The depositions contain mainly the elements:

- Oxygen
- Calcium
- Carbon
- Magnesium
- Potassium
- Silicium

Traces of the following elements are found:

- Aluminium
- Phosphor
- Sulphur
- Manganese
- Iron

# DTA-Measurement



Versuch	RAUCH5 [16.06.04]	Probe	Rauch-Pr5 114.00 mg	Kor. DTA
Tiegel	Pt	Ref.	Al2O3-Tiegel 0.00 mg	

# Conclusions

- Likely, the air preheater depositions are because of a chemical reaction rather than because of ash melting
- DTA measurements show an irreversible decomposition of the depositions at 700-900°C (air atmosphere).
- The carbonatisation reaction can be expected to happen at temperatures about 200-300°C lower than the decomposition temperature.
- Carbonatisation of CaO with flue-gas CO<sub>2</sub> likely to be the mechanism for deposits
- Next step: avoiding Ca in the process (Mg and Al as substitutes)



# Contact and Acknowledgement



[www.renet.at](http://www.renet.at)

[www.ficfb.at](http://www.ficfb.at)

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