The Fate of Trace Elements during Co-Combustion of Dried Sewage Sludge with Wood/Coal in a 12MW CFB Boiler

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This presentation:

- The research unit at CTH
- The test conditions
- The fuels
- Balance of ash and trace elements
- Ash distribution
- Concentration of trace elements in the ash
- Emissions of trace elements to the stack
- On-line measurement of Hg
- Conclusions

The Research Unit at Chalmers:



Stack measurements of trace elements



Hg total sampling in KMnO₄ solution

On-line measurement of Hg



Hg(total) - line

System for on-line measurement of elemental and total mercury in the flue gas duct

Principal runs

• Co-combustion with coal Test series one

• Co-combustion with wood-pellets, Test series two

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Operating conditions

				Coal, CTH	Wood, CTH
Load, MW				6.5±0.1	6.5±0.1
Bed temp.	°C (bottom)		841±0	841±0
Bed temp.	°C (top)			855±1	857±3
Exit temp,	after-burne	r chamber,	°C	772±4 (2)	797±1(782)(1)
Temp. at i	nlet of sec.	cyclone, °	C	150±0	150±0
Temp. inle	t of bag ho	use filter, °(C	150±0	150±0
Excess air	-ratio			1.23±0.01	1.23 ± 0.01
				4.05.0.04	4 0 4 0 0 4
Combusto	r air_ratio			1.05±0.01	1.04 ± 0.01
Superficiel				E 2 . O 4	
Superiiciai	velocity, n	1/5		5.3±0.4	$4.0\pm0.1(4.1)(2)$
	ddition Ca/	S molar rat	tio	2 2+0 05	
Calcium a				2.3±0.05	1.9±0.1(0)(1)
Ca/S with	Ca in fuel i			2 6+0 2	25+0.1(0)(1)
(1) without slu					

Measurements during the 48 h test

- Solids sampling (Fuel, cyclone leg, secondary cyclone, bag house filter and exit particles)
- Flue gas sampling (FTIR and heavy metals)
- In-situ gas sampling: downstream cyclone and in case of time on the furnace centreline

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Properties of the fuels

	Bituminous	Wood	Sewage
	coal	pellets	sludge
Proximate analysis			
Water (wt-%, raw)	8.6±1.1	9.2±0.2	19.0±5.4
Ash (wt-%, dry)	16.5±1.9	0.8±0.2	37.9±1.0
Combustibles (wt-%, dry)	83.5±1.9	99.2±0.2	62.1±1.0
Volatiles (wt-%, daf)	34.7±0.6	81.2±0.0	90.5±0.7
Ultimate analysis (wt-%, daf)			
С	82.5	50.5	53.2
H III	5.0	6.0	7.1
0	9.9	43.4	30.6
S .	0.90	0.02	1.90
N	1.70	0.14	7.10
CI	0.07	0.01	0.05
Lower heating value (MJ/kg)			
Hu, daf	32.49	18.91	20.9
Hu, raw	24.58±0.9	16.78±0.05	10.05±1.04
Trace elements (mg/kg dry fuel))		
Hg	0.073±0.03	<0.03±0	0.71±0.04
Cd	0.12±0.02	0.17±0.03	0.93±0.03
Pb	21±5	5±0	30±0
Cr	16±5	5±0	120±12
Cu	41±14	5±1.8	350±23
Mn	118±21	138±5	222±8.4
Со	5.8±1.5	3±0	7±0.6
Ni	19±3	2±0	26±1
As	1.6±0.5	0.3±0.0	4±0.1
Sb	0.4±0.06	0.3±0.0	1.3±0.4
V	39±2.9	0.2±0.2	27±4
П	0.09±0.01	0.02±0	0.078±0.005
daf= dry and ash free, raw=	as received		

Relative increase of trace elements to the CTH boiler



Comparison of relative increase of input flow of ash, Hg, Cr, Cu, Ni, V, Tl, as function of sludge supply

Relative increase of trace elements to the CTH boiler



Comparison of relative increase of input flow of Cd, Pb, Mn, Sb, As and Co, as function of sludge supply

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Recovery fraction, ash Out/In*100

Base fuel: Wood pellets



Recovery fraction, Hg, Pb, Cd, Cr, Cu, Ni

Base fuel: Wood pellets



Recovery fraction, Mn, Co, As, Sb, V, Tl



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Comparison of ash distribution

Base fuel: Wood pellets



Concentration of Hg in the ashes

Base fuel: Wood pellets



Concentration of Cd in the ashes

Base fuel: Wood pellets



Emissions of trace elements







Conclusions:

- Total mass and species balances have been made for co-combustion of sludge with both coal and wood as base fuel. In general a good closure is achieved.
- Both the influence of the increased ash content and the increased concentration of some trace elements in the sludge are reflected in the effluent ash streams.

Conclusions:

• The distribution of volatile trace elements, especially Hg, depends on the temperature. Especially important is the temperature of the separation devices for fly ash. In the present tests, the secondary cyclone and bag house filter capture even mercury (Hg).

Conclusions:

• The particle loading in the cold part of the gas path of a CFB and the content of carbon and/or CaO/CaSO₄ could be of importance for the capture efficiency of volatile trace elements but this needs to be further studied.