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Testing and Simulation in Turow Unit 3 and the Application of the Results on the Lagisza 460  $\rm Mw_e$  OT CFB

**Arto Hotta and Rafal Psik** 

**Foster Wheeler** 



# **Background for CFB Models**

- Trends for CFB boiler industry:
  - Larger unit sizes and higher steam parameters.
  - Higher efficiency.
  - Tighter emission standards.
- More detailed, fast and reliable models required.
- Valid model optimised CFB design and process performance.



### **Power Output of Foster Wheeler CFB Units**



### **PROCESS MEASUREMENTS IN TUROW UNIT 3**

#### EU PROJECT: Processes In Large-scale Circulating Fluidized Bed Combustors



•gas concentration

solids distribution

•temperature distribution

•solids flow

•solids segregation



### **PROCESS MEASUREMENTS IN TUROW UNIT 3**

#### **Gas concentrations**



# DESIGN MODEL FOR THE CFB HOT LOOP



# **Model Description**

- Steady-state combustion model for CFB furnace.
- 0-D fractional material balances.
- 3-D modeling of solid and gaseous species.
- 3-D modeling of energy balance.
- Empirical suspension density profile.

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# **Simulation Tools**

## The Dynamic CFB Model of Foster Wheeler

- A dynamic simulation tool to model dynamic behavior of the CFB system.
- Separate submodels have been developed for different parts of the CFB loop
  - Furnace
  - Solids separator
  - Return channel
  - INTREX<sup>™</sup> heat exchangers.

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 Each model component is based on the fundamental laws of conservation of mass, energy and momentum and on empirical correlations.

# **Analysis of Process Dynamics**

- Dynamic Process Tests
  - Dynamic process tests have been carried out in a 235 MW<sub>e</sub> CFB boiler.
- Process Modeling
  - A tailored dynamic simulator was built for the 235 MW<sub>e</sub> CFB boiler.
- Model Validation and Simulation Analysis
  - Measured data on the dynamic process tests were used to determine and to verify the model parameters and modeling principles.

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## Analysis of Process Dynamics Dynamic Process Tests

Test	Load	Load	Load	Load	
	100 %	80 %	60 %	40 %	
<b>Open loop load</b>	$100 \Rightarrow 90 \Rightarrow 80$	$80 \Rightarrow 70 \Rightarrow 60$	$60 \Rightarrow 50 \Rightarrow 40$	$40 \Rightarrow 50 \Rightarrow$	
change		$80 \Rightarrow 90 \Rightarrow 100$	$60 \Rightarrow 70 \Rightarrow 80$	60	
closed loop load	$100 \Rightarrow 80$	$80 \Rightarrow 60$	$60 \Rightarrow 40$	$40 \Rightarrow 60$	
change		$80 \Rightarrow 100$	$60 \Rightarrow 80$		
	4 %/min	4 %/min	4 %/min	4 %/min	
Fuel reactivity	+/- 10 %	+/- 10 %	+/- 10 %		
	step change	step change	step change		
Primary air	+/- 10 %	+/- 10 %	+/- 10 %		
	step change	step change	step change		
Secondary air	+/- 10 %	+/- 10 %	+/- 10 %		
	step change	step change	step change		
Prim/sec air	$60/40 \Rightarrow 65/35$	$60/40 \Longrightarrow 65/35$	$60/40 \Longrightarrow 65/35$		
ratio	$\Rightarrow$ 70/30 $\Rightarrow$	$\Rightarrow$ 70/30 $\Rightarrow$	$\Rightarrow$ 70/30 $\Rightarrow$		
	$60/40 \Longrightarrow 55/45$	$60/40 \Longrightarrow 55/45$	$60/40 \Longrightarrow 55/45$		
	$\Rightarrow$ 50/50 $\Rightarrow$	$\Rightarrow$ 50/50 $\Rightarrow$	$\Rightarrow$ 50/50 $\Rightarrow$		
	60/40	60/40	60/40		

Matrix of the Dynamic Process Tests

## Analysis of Process Dynamics Dynamic Process Tests



## Analysis of Process Dynamics Basics of the CFB Dynamics



### **HIPE CFB**

High Performance Multifuel CFB with Advanced Steam Cycle

- EU funded research program (2001 2003)
  - Total volume 3.6 M€(1.7 M€from EU)
- Objective
  - Development of Supercritical Once Through Design for Circulating Fluidized Bed (CFB) Boiler
- Partners
  - Foster Wheeler Energia OY
  - Siemens AG
  - Energoproject Katowice
  - Technical Research Center of Finland



Lagisza Power Station, 460 MW<sub>e</sub>, Poland

#### **CFB BOILER DESIGN DATA**

Output		MWe		460		
Steam Flow		kg/s (SH/RH) 36		360/313		
Steam Pressure		bar (SH/RH) 275/50		275/50		
Steam Temperature		°C (SH/RH) 565/580				
SCHEDULE		•	2			
Contract Signing		December 30, 2002				
Engineering Release		March 1, 2003				
<b>Mechanical Completion</b>		February 28, 2006				
<b>Commercial Operation</b>		September 30, 2006				
FUELS (as received)		Coal	Соа	al Slurry (max. 3	0 %)	
	F	Performan	ce Range	Range		
Sulphur	% wt	1.2	0.6 – 1.4	0.6 – 1.6		
Ash	% wt	23	10-25	28-65		
Moisture	% wt	12	6-23	27-45		
LHV	MJ/kg	20	18-23	7-17		

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### Lagisza: Evaporator Studies

- Furnace calculated with Foster Wheeler's modern 3D furnace model
- Different design conditions evaluated
  - Furnace conditions
  - Evaporator water/steam side conditions
  - Example: Coal feeder disturbance



#### HEAT FLUX COMPARISON



- Low and uniform heat fluxes in a CFB furnace
- Lower mass flow rates ("natural circulation characteristics")









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### **SUMMARY**

Process tests in Turow produced valuable data for the modelling of large scale furnaces

The valid models are essential tools in further development of OT CFB (Lagisza)

The models are tools for the further optimisation of Turow units

