

Capacitance effect of porous bed material - an approach to improve conversion of volatile matter within fluidized bed -

T. Shimizu, S. Kanou, J. Asazuma,
H. Takagi, K. Yamagiwa
Niigata University, Japan

N. Fujiwara, T. Teramae
Idemitsu Kosan Co. Ltd, Japan



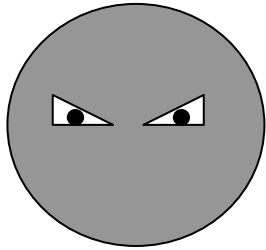
Background of the present work

- Biomass (or plastics, municipal wastes, sludge, etc.) : **High volatile matter fuels**
- High conversion of V.M. is important to attain high plant efficiency. However, conversion of V.M. in the dense bed is often poor since V.M. evolution occurs at upper surface of the dense bed.
- Insufficient conversion of V.M. results in troubles such as **tar deposition** and **dioxin formation** in back-pass.

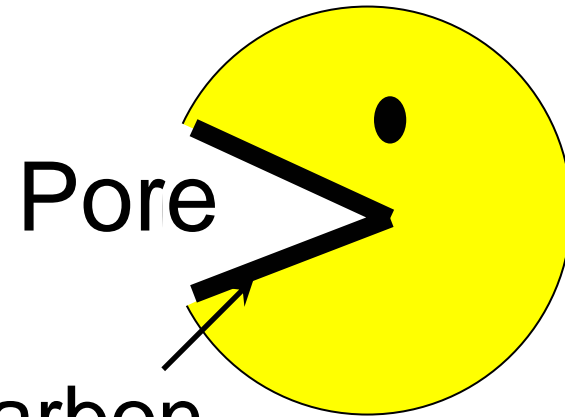


An approach to improve V.M. conversion: capacitance effect

V.M., tar



Porous solids



Pore

Carbon

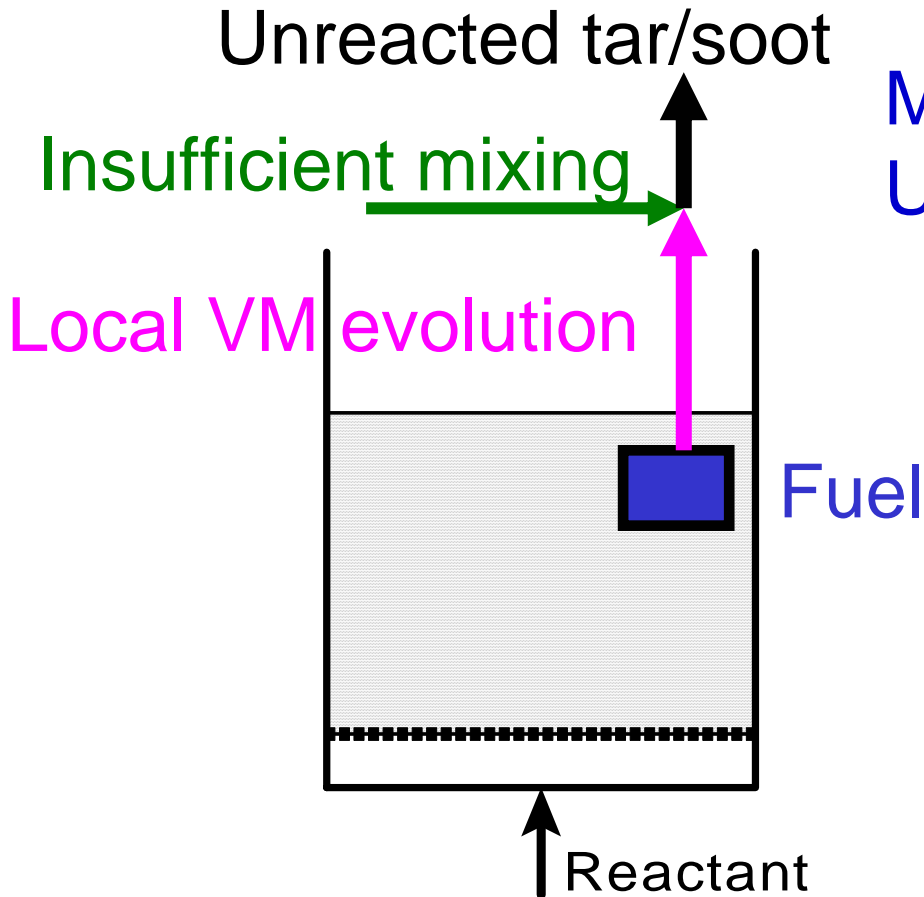
Porous particles capture V.M. at high temperatures; carbon deposit is formed within pores.

→ Increased residence time of V.M.



Expected advantages of porous bed material in comparison to sand bed

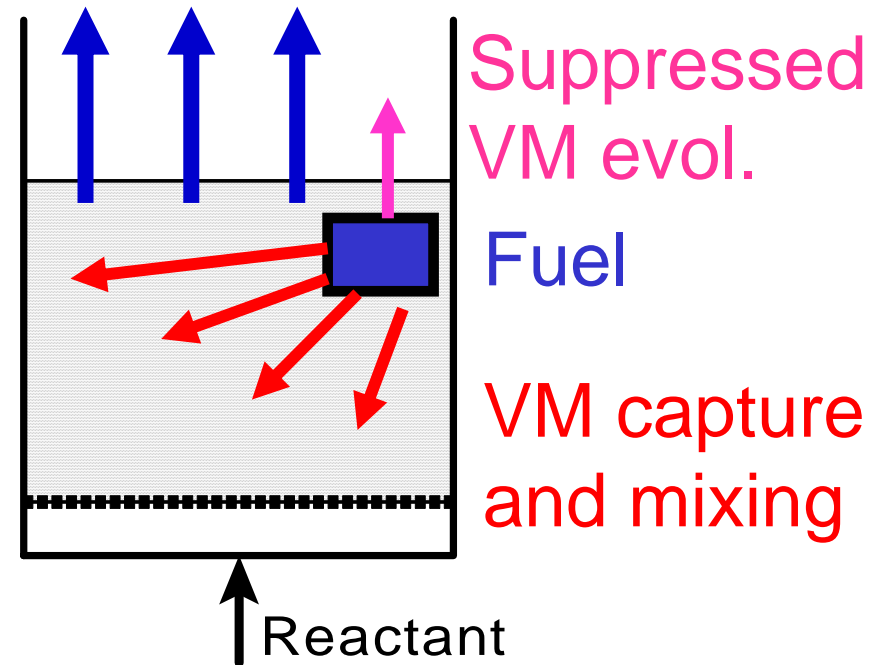
Conventional sand bed



(a) Sand bed

Porous particle bed

More reaction in bed
Uniform product formation



(b) Porous particle bed



Improved horizontal dispersion by porous bed material during plastic pellet combustion

Total carbon

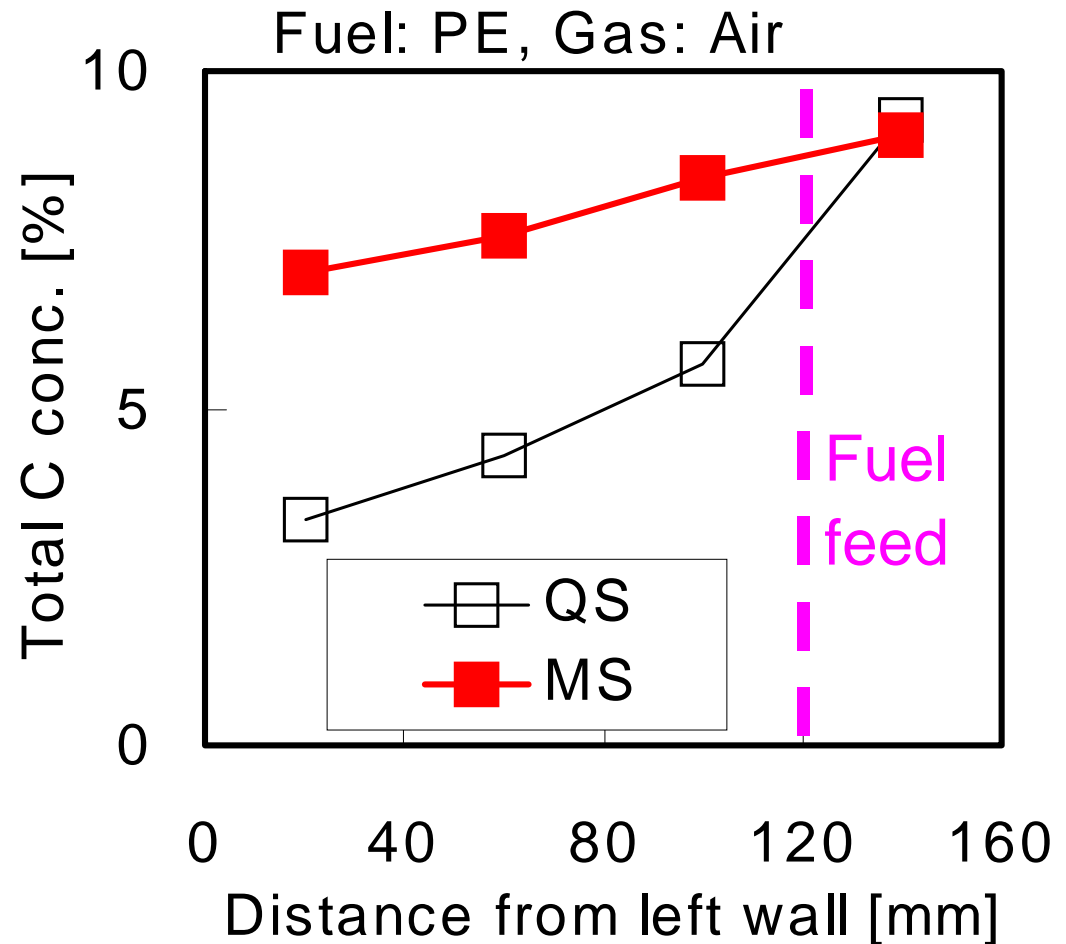
=CO₂+CO

+CH₄+2C₂H_n+...

measured in
freeboard

QS (non-porous):
non-uniform gas
dispersion

MS (porous) : uniform
gas dispersion



Shimizu, J. Japan. Inst.
Energy, 80, 333 (2001)

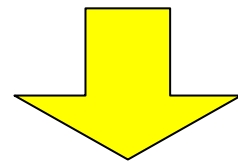


Reaction rates are not yet available!

For the rational design of reactors, reaction rates are necessary.

1) volatile matter capture

2) removal of carbon deposit from the bed material by combustion or gasification



Kinetic study was conducted in this work.



Present work

- Volatile matter capture by porous bed materials was conducted in an inert atmosphere at 650 - 850 °C using a fixed bed reactor.
- Burning rate of the carbon deposit over porous bed material was also measured.



EXPERIMENTAL



Porous bed materials

	MS	MS-1B	Activated Bauxite
Size	0.75 mm	0.4 mm	0.4 mm
Al ₂ O ₃	91.32	84.7	69.4
SiO ₂	n.a.	2.2	7.2
MgO	0.15	0.0	0.0
CaO	0.07	0.8	0.3
TiO ₂	n.a.	1.1	13.0
Fe ₂ O ₃	0.54	5.8	8.4
SO ₃	2.10	3.8	0.8
Others	n.a.	1.6	0.9
Area [m ² /g]	187	195	124

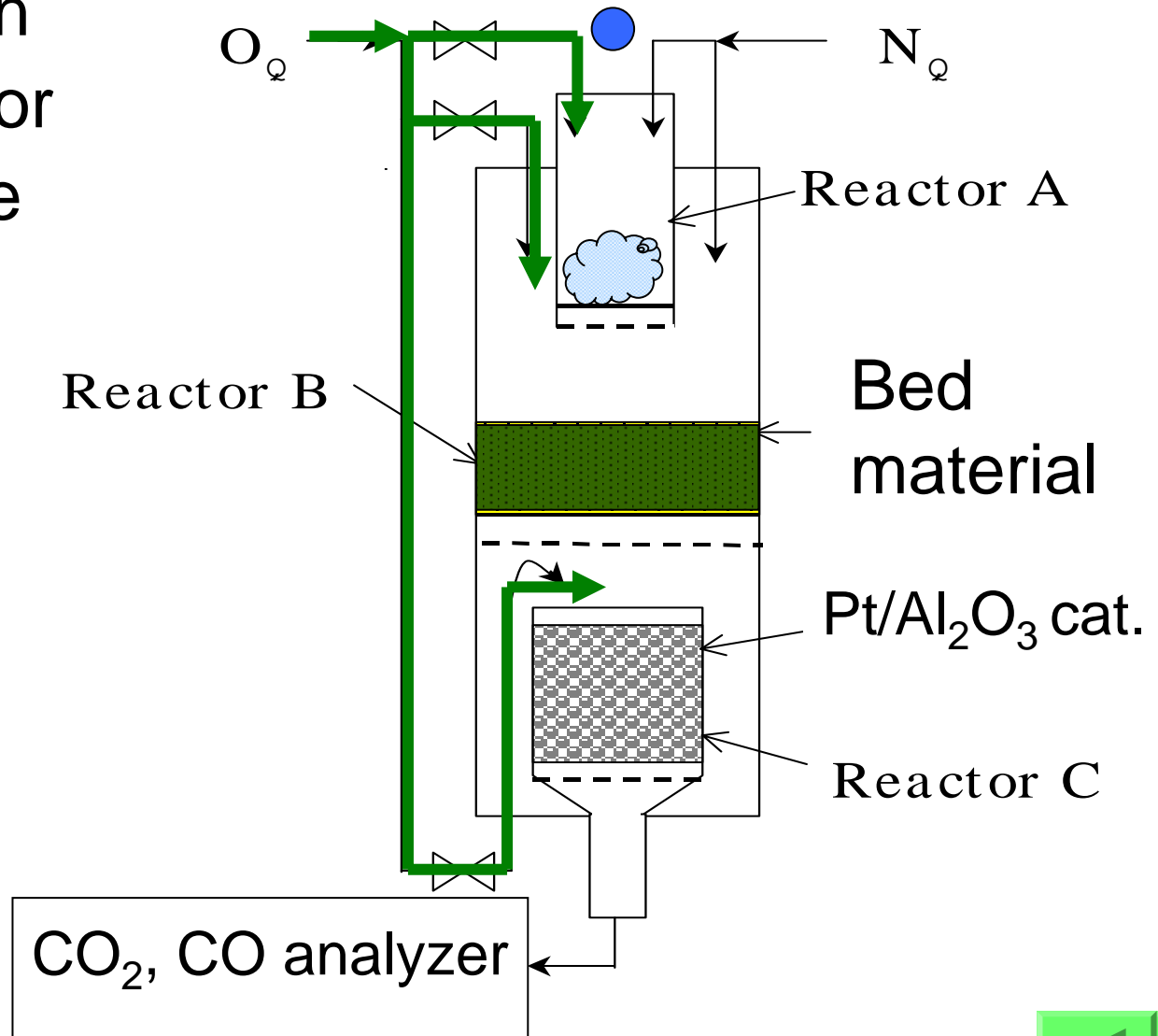


Fixed bed reactor

Step1: Evolution of V.M. in reactor A. V.M. capture in reactor B.

Step2: Deposit combustion.

Step3: Char combustion in reactor A.



Experimental conditions

Temperature: 650 – 850 °C

Reactor i.d.: 27 mm

Solid bulk volume: 26 cm³

Total gas flow rate: 2.2 NI/min

Fuel: Polyethylene (V.M. 100 %)

O₂ concentration during deposit
carbon combustion: 7- 21 %



RESULTS AND DISCUSSION

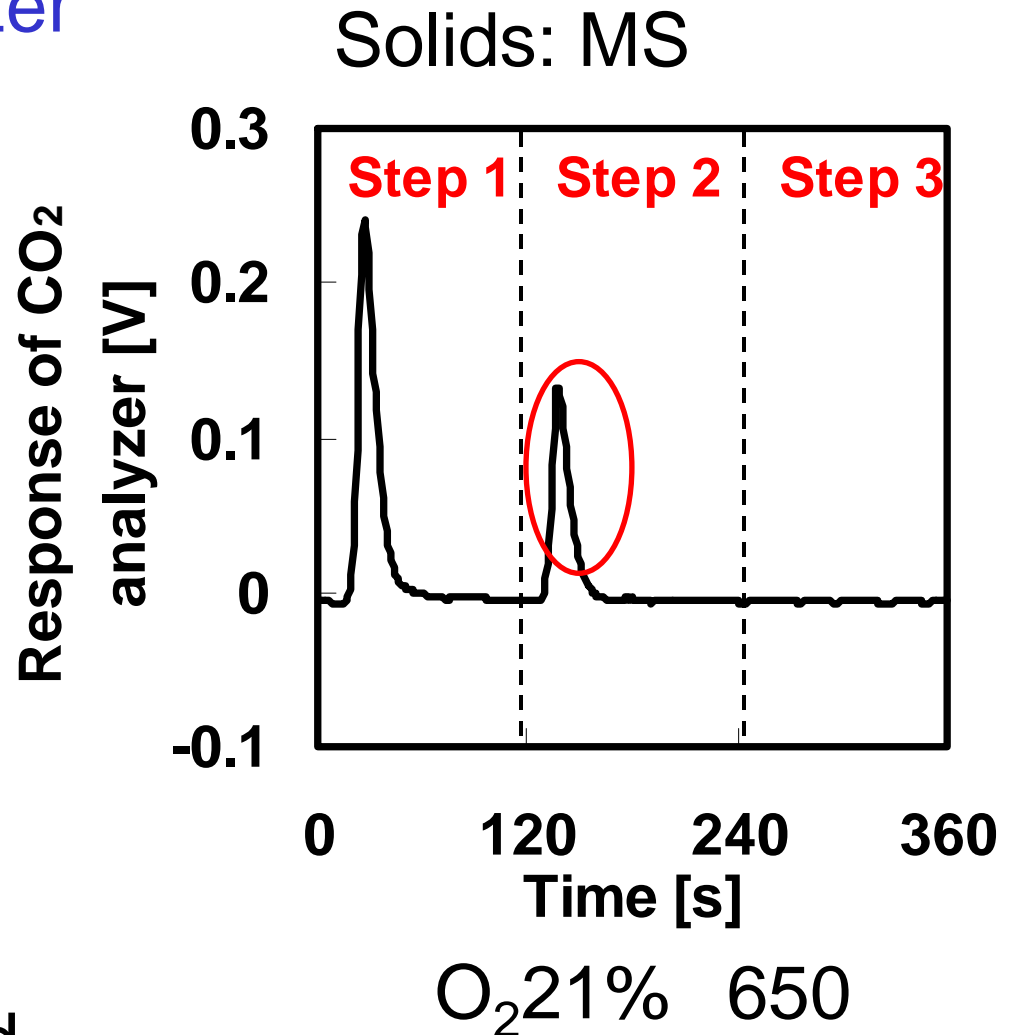


A typical result of fixed bed study

Signal from CO₂ analyzer

- 1: V.M. evolution (Part of V.M. was not captured by solids.)
- 2: Deposit combustion
- 3: Char combustion

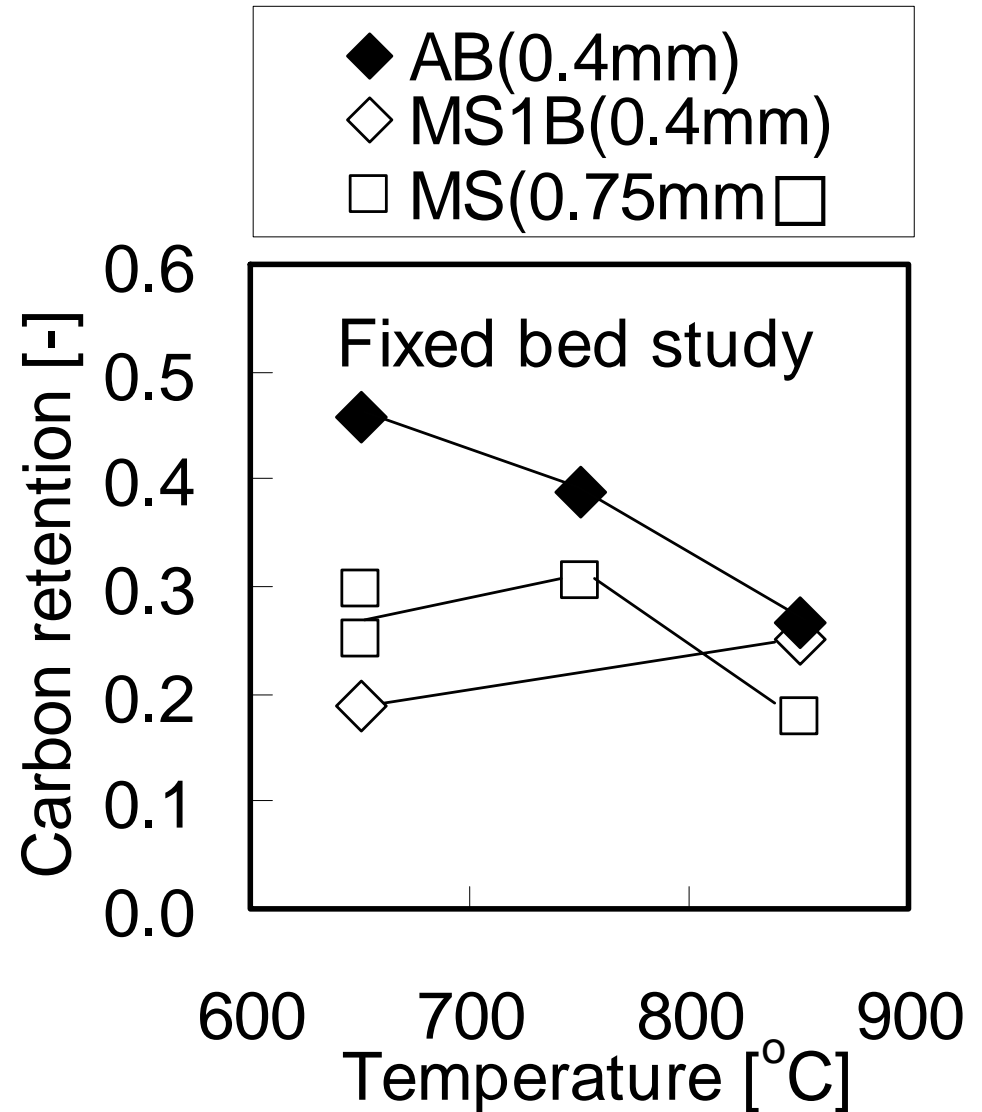
From CO₂ formation during step 2, the amount of carbon deposit was determined.



Effect of temperature on V.M. capture

Carbon retention
=(deposit)/(feed)

Carbon retention
and the effect of
temperature on it
differed among
bed materials.

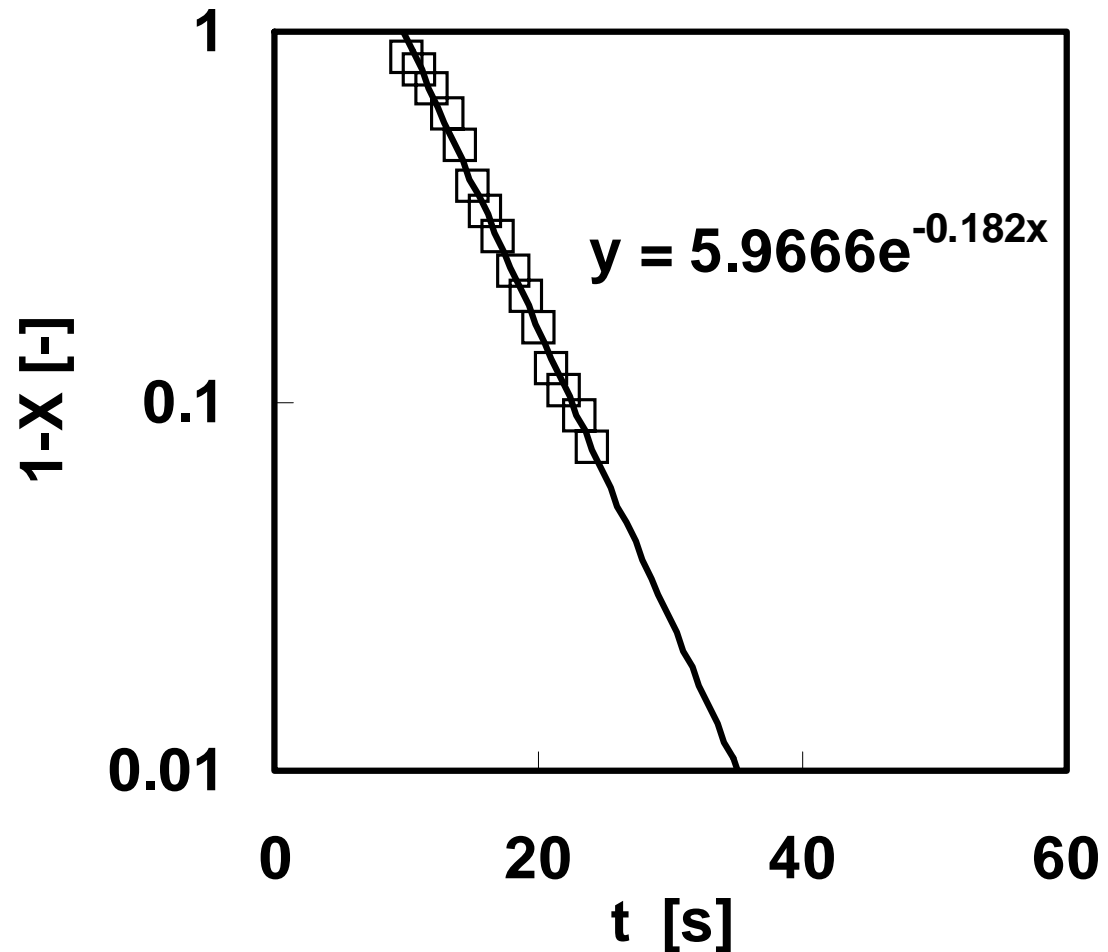


Burning rate of carbon deposit

Burning rate of carbon deposit was measured at O₂ concentration 7 -21 and 650 - 850 °C.

Reaction rate was given as follows:

$$dX/dt = k(1-X)$$

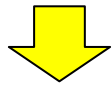


(MS 0.75mm, O₂21%, 650)



Effect of O₂ concentration on k

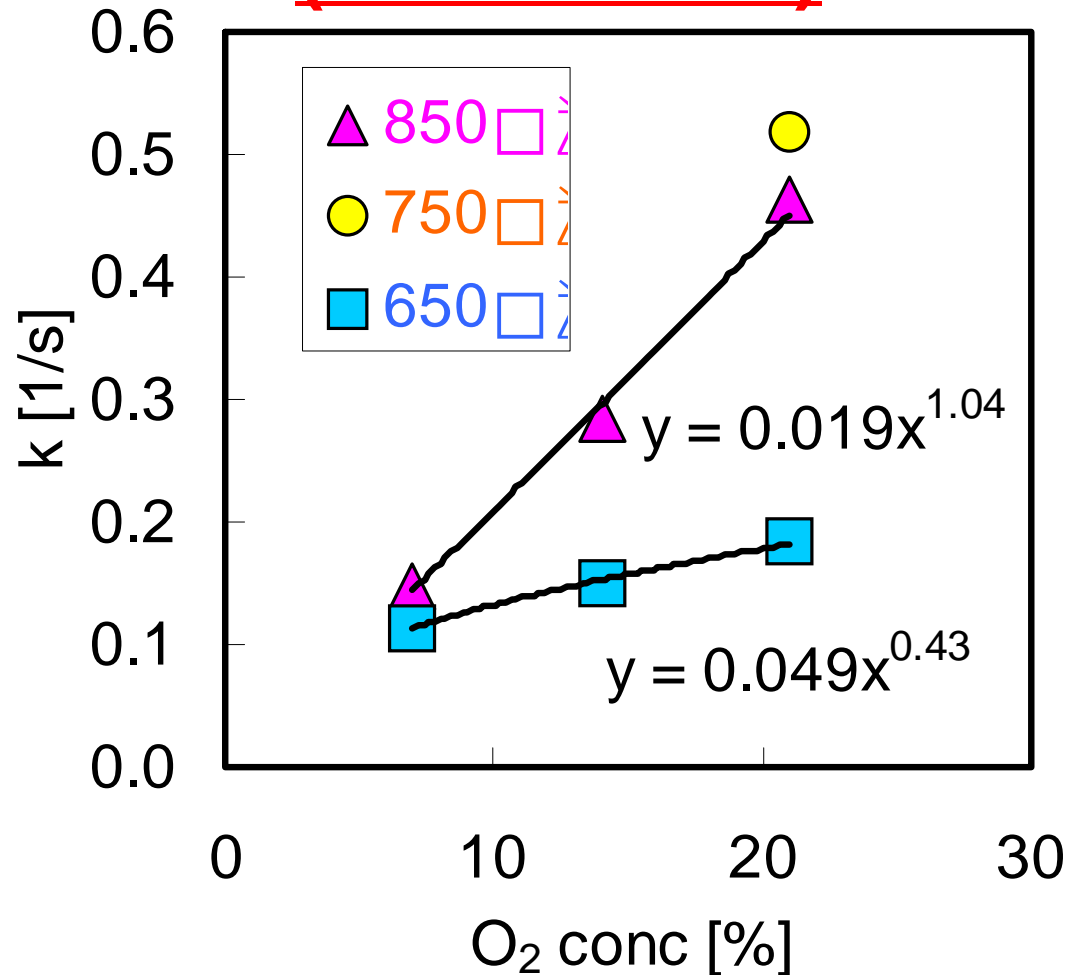
No increase in k with increasing temperature from 750 to 850 °C.



Diffusion controlling at temperatures above 750 °C

At 650 °C, reaction order with respect to O₂ was 0.43.

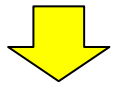
(MS 0.75mm)



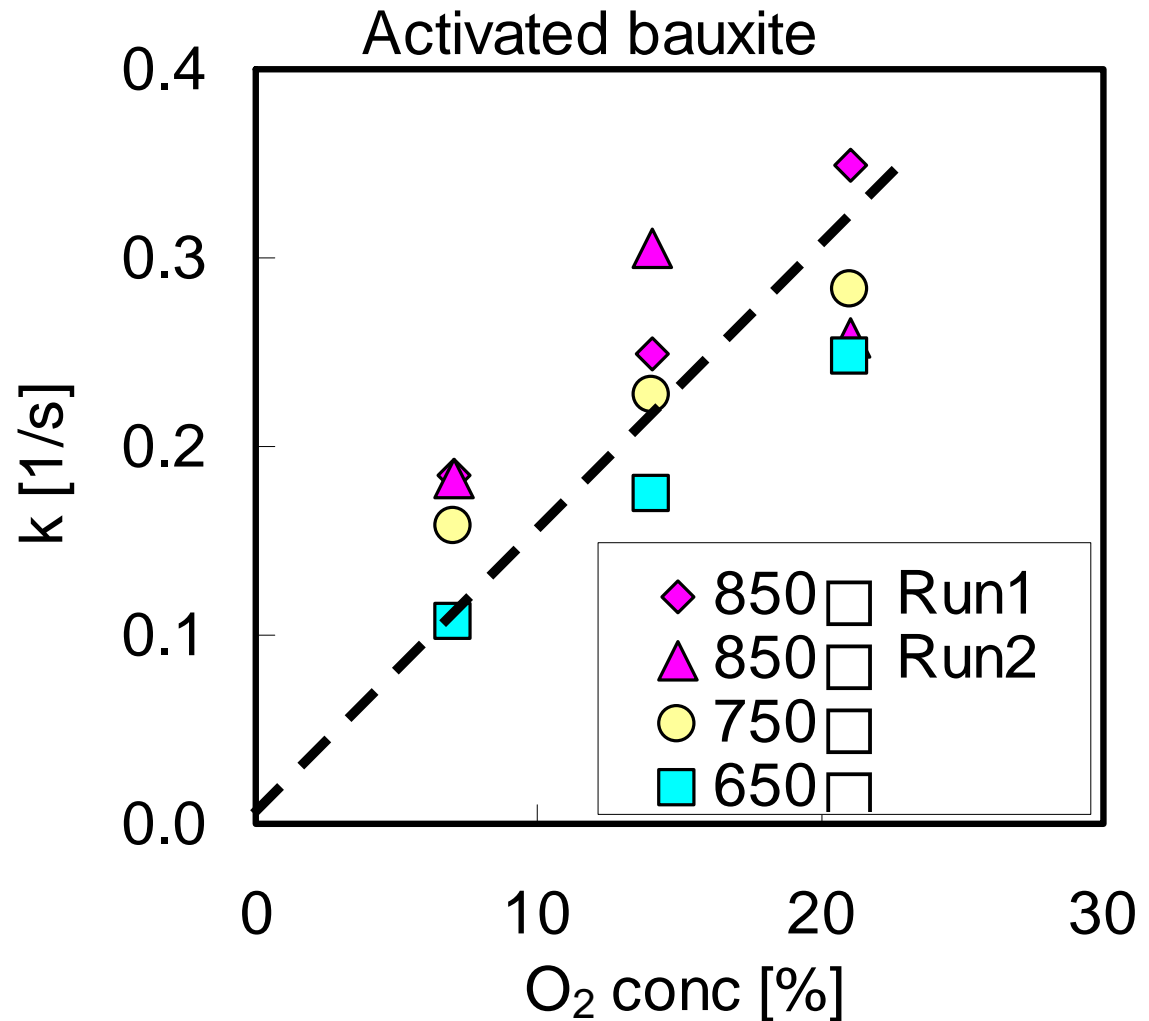
Effect of O₂ concentration on k

AB (0.4 mm)

No increase in k
with increasing
temperature from
650 to 850 °C.



Diffusion controlling
at temperatures
above 650 °C



CONCLUSION

An experimental procedure was proposed to evaluate the volatile matter capture by porous bed materials and its regeneration rate.

V.M. capture by porous bed material

- The effect of temperature on carbon retention depended on type of bed material.

Burning rate of carbon deposit

- Carbon burn-up rate differed among bed materials.



ACKNOWLEDGEMENT

This work was financially supported by The New Energy and Industrial Technology Development Organization (NEDO), Japan.

